

Removal of acid red 88 from wastewater by adsorption on agro-based waste material. A case study of Iranian golden *Sesamum indicum* hull

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Abstract

Background: Colors are very useful in different industries such as textile and leather but when they enter water, can cause many biological and environmental problems. In the present research, a waste agricultural material which is freely available is employed to analyze its efficiency for removing acid dye from contaminated wastewaters.

Methods: In this study, batch adsorption experiments were performed in the treatment process of acid red 88 (AR88) by Iranian golden *Sesamum indicum* (IGSI) seeds hull which is produced abundantly in some countries and especially in Iran up to 1100 kg/ha. Also, the effect of operational parameters like adsorption time, pH, dye concentration and adsorbent dosage was studied on pollutant removing efficiency. The experimental data of AR88 adsorption was fitted to Langmuir, Freundlich and Temkin isotherm models. The scanning electron microscopy (SEM) images for the IGSI were taken before and after adsorption process.

Results: The efficiency of dye adsorption on adsorbent was found to be 98.2%. The optimum pH for treatment was 4.5 which is in the acidic range. Enhancing the adsorbent dosage from 0.5 to 2.5 g caused increasing in removal efficiency from 73.85% to 95.85%. Decreasing in dye concentration from 70 to 30 mg/L caused increasing in removal efficiency from 79.73% to 95.83%. The process of adsorption was best fitted to Langmuir model and the amount of dye adsorbed on adsorbent, q_e , was found to be 25 mg/g. Comparison between SEM images before and after dye adsorption, showed the significant difference that was due to the dye loading on adsorbent.

Conclusion: The results of present study demonstrated higher dye removal efficiency for AR88 in acidic pHs. Employing the IGSI material in this study proves to be a potential alternative to expensive adsorbents, utilized for the treatment of contaminated industrial waste waters.

Keywords: Adsorption, Acid red 88, Waste products, *Sesamum*, Waste water, Color removal

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Introduction

One of the most evident contaminants in water are colors and they come to water bodies from different sources such as textile and leather industries and from painting products in other industries. Color prevents light pervasion in water so decreases photosynthesis and disorder growing of biota. Because of composing chelate by metal ions produce micro-toxicity to fish and other organisms (1,2). The release of azo dyes into the environment is a concern due to coloration of natural

waters, toxicity, mutagenicity and carcinogenicity of these dyes and their bio-transformation products (3,4). Some dyes under anaerobic conditions in wastewater, may decompose into carcinogenic aromatic amines and cause serious malady to men and animals (5,6). Due to complex molecular structure, dyes are usually persistent against biodegradation, and thus it is difficult to eliminate them by natural aquatic environment (7,8). And these poisonous materials absorb the oxygen of water (9,10). The common decolorization methods for synthetic dyes are



coagulation, flocculation, microbiological or enzymatic decomposition, adsorption, membrane filtration, ion-exchange, oxidation and advanced oxidation (11). Because of the fact that every method has its own elimination, as an alternative, agricultural waste materials are inexpensive, freely available, abundant, having simple application, high efficiency and green chemistry. Then developing countries are eager to use them in order to treat industrial wastewaters (12-14). Many nonconventional, low-cost adsorbents such as jute stick powder (15), cattail root (16), *Azadirachta indica* leaf powder (17), jute processing wastes (18), peanut hull (19), orange peel (20), coir pith (21), bagasse pith (22), hardwood sawdust (23) and hazelnut shells (24) have been widely used for wastewater treatment in research areas. Harmless adsorption way by agricultural wastes, conducted us to use a novel adsorbent for removing pollutants from waste water. Thus, it is a good choice to remove synthetic dyes before they discharge downstream bodies of water. In this research, we studied the ability of *Sesamum indicum* seed's waste which is being produced annually in Iran, known as Iranian Golden *Sesamum indicum* (IGSI) for adsorption of acid red 88 (AR88) from simulated wastewater. *S. indicum* is a flowering plant in the genus *Sesamum*, also called *benne*. It is widely naturalized in tropical regions and Middle East countries and is cultivated for its edible seeds, which grow in pods or "buns". The world, harvests million tons of *S. indicum* seeds every year, and has many nutritional and nutraceutical properties (25,26). *S. indicum* belongs to the family *Pedaliaceae*'s which is estimated to have 36 species (24). But their wild species exist in Africa and a few in India (25). The origin of this plant is known in Ethiopia (27). Because of high nutritive quality and stability, *S. indicum* oil is known as a rich food (28). It has different usages and it clearly differs from other oils extracted from vegetables, because of its high nutritional and therapeutic values. The seeds of this species contain 50%-60% oil, 18%-25% protein, 13.5% carbohydrate and 5% ash (29). *Sesamum* has antioxidative, anticancer, anti-hypersensitive and anti-immunoregulatory actions (30). The considerable stability of the seeds to oxidation can be due to its endogenous antioxidant lignin along with tocopherols (29). *S. indicum* is a natural source of Calcium (approximately 1%) and phosphorous (approximately 0.7%) (28). *S. indicum* contains plenty amounts of oleic (43%), palmitic (11%), stearic acid (7%) and linoleic (35%) which together include 96% of the total fatty acids (25). *S. indicum* seeds have different sizes and colors. They vary in size from small to large and are found in range of distinctive colors, depending upon the variety, including white, grey, black, golden and red (27). Especially in the eastern parts of the world, *sesame* has long been considered as a seed which provides high energy and prevents ageing (31).

Per capita production of this plant in Iran is doubled its world average production, equal to 1100 kg/ha. So it is available and inexpensive, and using its waste perfects its abilities (32). Finally the potential of IGSI as an agro-

based waste material for removing the pollutant, AR88, by testing different parameters such as initial amount of adsorbent, pH, initial dye concentration, adsorption time and studying the isotherm models was the aim of this study.

The results suggest a highly economical adsorbent for the removal of AR88 from wastewater. Additionally, this study helps to improve the removal efficiency of AR88 in comparison to other similar methods.

Materials and Methods

The preparation of the adsorbent (IGSI) and the adsorbate (AR88)

Sesamum indicum seed waste was collected as a solid waste which was obtained from a local oil-pressing shop in Tabriz. It was free of charge. Figure 1 shows the IGSI after being oil-pressed by its especial apparatus. The waste material was washed with distilled water for several times, and put in oven at 60°C for 4 hours. Then, the sample was ground completely with a mortar and pestle and then boiled for five times in distilled water to remove the residual oil and other unwanted materials and dirt particles. The washed material was dried in a hot air oven at 60°C for 48 hours. Then, the sample was ground completely again and the final sample was stored in an airtight plastic bottle for further use in room temperature. The dye used in this study was AR88 ($C_{20}H_{13}N_2NaO_4S$, molar mass 400.38 g/mol) which was obtained from Sigma-Aldrich corporation. The chemical structure of the dye is presented in Figure 2. As it was observed in UV-Vis spectrum (UV-Vis spectrophotometer, Jinan Hanon instruments, Model: i3) the maximum absorbance wavelength, λ_{max} , was at 507 nm. The stock solution (1000 mg/L) of AR88 was prepared by dissolving an accurate weight amount of dye in distilled water and the other concentrations were obtained by diluting this stock solution using the following formula:

$$M_1V_1 = M_2V_2 \quad (1)$$

The experiments were performed according to Khataee and Kasiri (33). 400 mL graduated cylinder containing 300 mL dye solution was utilized, in which the adsorbent was added. For more precision the experiments were done



Figure 1. *Sesamum indicum* seeds after being oil-pressed.

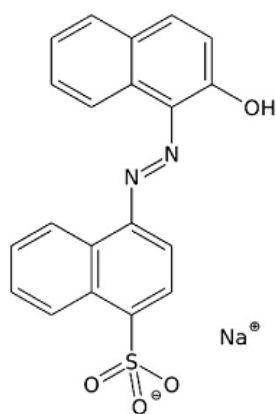


Figure 2. Chemical structure of acid red 88.

by two graduated cylinders containing equal amounts of adsorbent and dye concentration. UV-Vis results of both of them were obtained and the average was reported. Because of the fact that in present study the samples were taken every 5 minutes, and it had time delay to deposit the IGSI particles, the Graduated Cylinder was utilized in order to its height. Then the sampling of dye solution was easier and free from any adsorbent particles. The system was put on a magnetic stirrer (Hotplate & Stirrer, JENWAY 1000) at a fixed stirring rate of 300 rpm. All the samples were centrifuged (Select-a-fuge 24 BIO-DYNAMICS) to deposit the trifle adsorbent. The rate of centrifuge was fixed on 5000 rpm for 5 minutes. The batch removal experiments were carried out at different initial dye concentrations (30–70 mg/L), adsorbent weights (0.5–2.5 g), reaction time (5–170 minutes) and pH values (2.5–10.5), to evaluate the effects of operational variables on the dye removal efficiency. The desired pH was adjusted using 0.1 mol/L HCl and 0.1 mol/L NaOH by pH meter (654 pH meter Metrohm, Switzerland). At regular time intervals during adsorption process, 16 samples of the dye solution were totally taken, in each experiment and filled in test tubes which were put in test tube rack respectively. All the experiments were done at $T=25^{\circ}\text{C}$. Dye removal efficiency (%) was expressed as the percentage ratio of decolorized dye concentration to that of the initial concentration as shown in the formula (33).

$$\% \text{Dye Removal (DR\%)} = \frac{C_i - C_f}{C_i} \times 100 \quad (2)$$

The amount of dye adsorbed at equilibrium q_e (mg/g) was calculated by:

$$q_e = C_i - C_f \times \frac{V}{M} \quad (3)$$

where C_i and C_f are the initial and final liquid phase concentrations (mg/L). The volume of acid dye solution, V in (L) and the adsorbent mass (g) is given by M . Scanning electron microscopy (SEM) (Sirion 200, FEI Co., Holland) was used to image the IGSI adsorbent before and after adsorption at a magnification of $\times 1000$.

Equilibrium adsorption isotherms are of fundamental

importance in the design of adsorption systems. In this study, three isotherm models were selected to describe the adsorption of AR88 onto IGSI at 25°C . These isotherm models include the Langmuir, Freundlich and Temkin models, and adsorption intensity R_L (Eq. 4) was also selected to describe the adsorption.

$$R_L = \frac{1}{1 + KC} \quad (4)$$

The R_L values indicate that the adsorption process is irreversible when R_L is 0, favorable when R_L is between 0 and 1, linear when R_L is 1 and unfavorable when R_L is greater than 1 (34,35).

Results

Effects of operational parameters on adsorption process

Effect of initial amount of adsorbent

In order to make a comparative study for adsorption of AR88 solution in the presence of different quantities of IGSI (0.5–2.5 g/0.3 L), the initial concentration of AR88, reaction time and pH were kept constant. Figure 3 shows the effect of different weights of IGSI on adsorption of AR88 solution. It is clear that, dye removal significantly increased as the adsorbent weight increases.

Effect of initial dye concentration

Adsorption of dye on the adsorbent surface was determined for different concentrations of AR88 on 1.5 g of IGSI. According to the results, increasing the initial dye concentration, reduced the dye removal efficiency over the same time interval as shown in Figure 4.

Effect of initial pH

The effects of pH on acid dye adsorption have been studied by many researchers, and the results indicated that, pH of solution could significantly influence the adsorption process (36,37). Also in present experiment the effect of initial pH of solution was analyzed on adsorption efficiency. Hydrochloric acid was used to adjust the pH in lower levels and Sodium Hydroxide was utilized to adjust it in higher levels of pH. Among pH ranges of dye solution (2.5–10.5) containing 50 mg/L dye, the adsorption

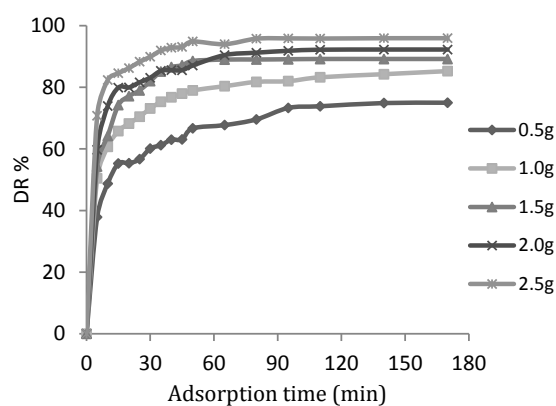


Figure 3. Effect of different IGSI weights on adsorption of AR88 (pH = 6.5, [AR88] = 50 mg/L, reaction time = 170 min).

efficiency was approximately significant in the pH = 4.5 as has been shown in Figure 5. The results indicated that the adsorption increases as the pH value is around acidic pHs. According to the result of pH effects, we suggest the following mechanism for probable reaction between dye and adsorbent which is described in Figure 6.

The adsorption mechanism can be easily evaluated by determining the point of zero charge on adsorbent surface (38,39). In this study the $\text{pH} > \text{pH}_{\text{pzc}}$ helps to increase the adsorption of cations while the $\text{pH} < \text{pH}_{\text{pzc}}$ helps to enhance the adsorption of anions. Solid addition method (40) was used to determine the point of zero charge of IGSI which was found to be 7 respectively. These are shown in Figure 7. In addition to mentioned experiments, another analysis was performed in order to find the effect of pH on dye solution which was free from any adsorbent. In this analysis the pH of pure dye solution was changed from 2.5 to 10.5. The results showed that there was no any sensible decolorization in pH range variation. Then by all these observations it is concluded, that the pH plays its role by effecting on adsorbent and causes different dye removal efficiencies in pH ranges (41).

Effect of reaction time

The effect of reaction time on dye removal efficiency was evaluated while the initial concentration of AR88, initial

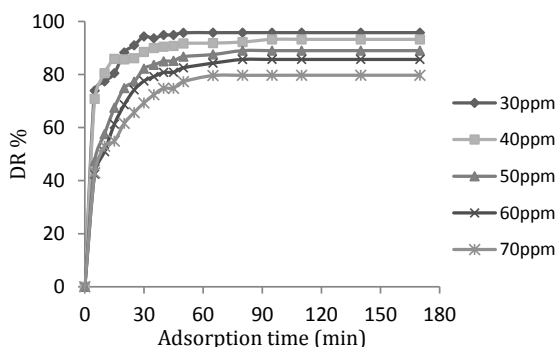


Figure 4. Effect of initial concentration of AR88 on removal efficiency (pH = 6.5, adsorbent weight = 1.5 g, reaction time = 170 min)

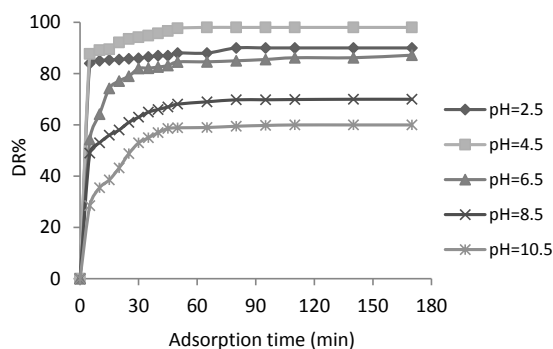


Figure 5. Effect of pH on adsorption of AR88 (adsorbent weight = 1.5 g, [AR88] = 50 mg/L, reaction time = 170 min).

pH and IGSI weight were kept constant. Dye removal increased as reaction time was enhanced. Figures 3 and 4 also show the relation between reaction time and dye adsorption efficiency.

Surface characteristics of IGSI (before and after adsorption)

The SEM images captured for the IGSI adsorbent before and after dye adsorption are respectively shown in Figures 8A and 8B. Before pollutant adsorption, the IGSI had a surface which was rough with heterogeneous pores and cavities, that indicated there was a good feasibility for AR88 to be trapped and adsorbed onto the surface. Because these pores and cavities supply a large exposed surface area. After adsorption, the surface of adsorbent was comparatively smoother, implying that AR88 molecules had become attached to the IGSI surface.

The equilibrium adsorption isotherms

In order to study the isotherm data for adsorption of AR88 onto the adsorbent, the Langmuir, Freundlich and Temkin models were analyzed and observed (42). Experimental results achieved for AR88 adsorbed onto IGSI at 25°C fit well to the three isotherm models. The equilibrium data were best represented by the Langmuir isotherm model and the plot between C_e/q_e and C_e yielded a straight line with a high correlation coefficient ($R^2 = 0.9842$). The R_L values for the adsorption of AR88 onto IGSI were in the range of 0.05–0.11 when the initial AR88

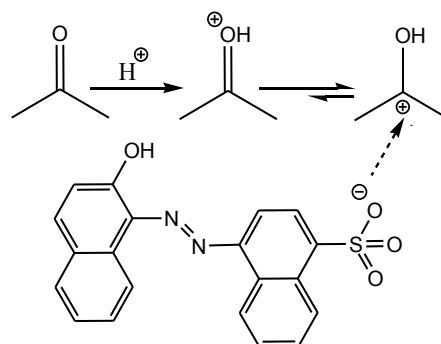


Figure 6. The schematic of suggested probable reaction between dye molecule and adsorbent surface.

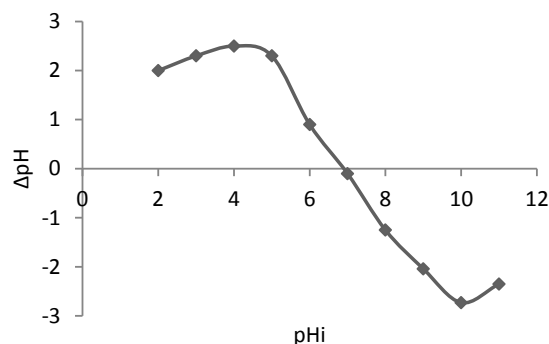


Figure 7. Point of zero charge of *Sesamum indicum* hull.

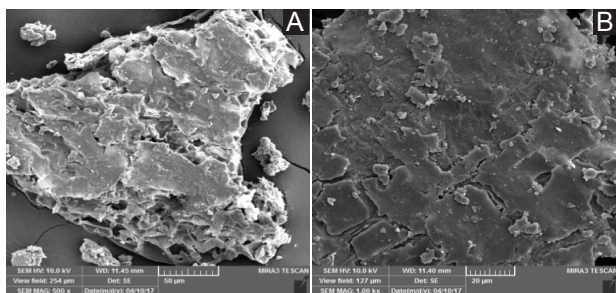


Figure 8. SEM micrograph of untreated (A) and dye-loaded (B) hull at the magnification of $\times 1000$.

concentration varied from 30 to 70 mg/L. This indicates that the adsorption is a favorable process. The obtained parameters of mentioned isotherms, using the linear form of the isotherm equations are given in Table 1. The amount of dye adsorbed on adsorbent, q_e , was found to be 25 mg/g. The Freundlich isotherm constants were determined from the linear form of the model, and the values of K_f , n and the correlation coefficient are given in Table 1. The Temkin isotherm constants for adsorption of AR88 onto IGSI calculated from the plot of q_e vs $\ln C_e$ are given in Table 1 (42). The comparative fits of experimental data for adsorption of AR88, onto IGSI are shown in Figures 9, 10 and 11.

Discussion

Increasing the DR% as enhancing the weight of adsorbent which is obvious in Figure 3, is because of the fact that increasing the amount of adsorbent provides more surface area for adsorption of dye molecules on the surface of *S. indicum* seed's hull (34). As the analysis around evaluation of the effect of dye concentration showed, increasing in concentration, resulted a reduction in removal efficiency. This can be due to the fact that there are only limited parts on the adsorbent surface to adsorb the dye, and as the concentration of AR88 is increasing, the chance of dye molecules for being adsorbed will be decreased (35). In pH analysis, the reason that influences the adsorption efficiency can be due to the fact that *S. indicum* hull contains hydroxyl groups as well as carbonyl groups, as determined using FTIR analysis (38). Therefore, the effect of pH on adsorption of AR88 onto IGSI might be attributed to electrostatic attractions. Electrostatic attractions may operate over a large range of pH (here from pH 2.5 to pH 10.5) (39). At low pH values, the excessive H^+ ions may enter in a reaction with carbonyl groups and a new positive part generates on oxygen. Due to the fact that the positive charge is not stable on oxygen, it absorbs the bonding pair electrons and neutralizes. The conjugate carbon changes into a carbocation. This positively charged carbon, is now ready to be attacked by the anionic site of the dye. As the schematic of probable reaction was described in Figure 5. The point of zero charge showed that the adsorption capacity of *S. indicum* hull was enhanced by decreasing the pH of solution below pH_{pzc} . The reason might be the protonation of surface functional groups of adsorbent

Table 1. Isotherm parameters for the adsorption of AR88 onto IGSI

Isotherm model	Parameter	Quantity
Langmuir	q_{max}	25
	B	0.26
	R^2	0.9842
Freundlich	K_f	10.11
	n	4.30
	R^2	0.8747
Tempkin	B	4.03
	K	8.08
	R^2	0.8841

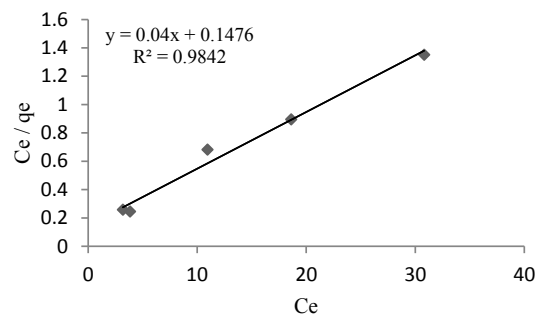


Figure 9. Fit of Langmuir isotherm data for the adsorption of AR88 onto IGSI.

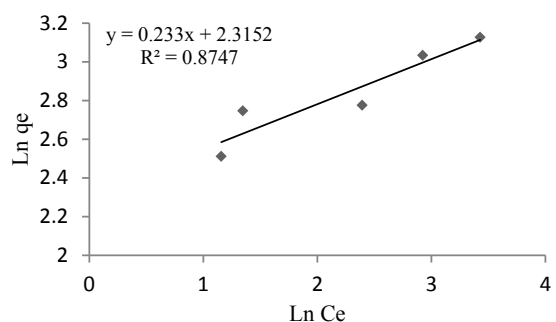


Figure 10. Fit of Freundlich isotherm data for the adsorption of AR88 onto IGSI.

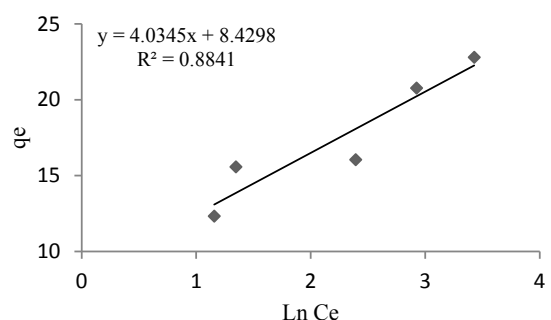


Figure 11. Fit of Temkin isotherm data for the adsorption of AR88 onto IGSI

at low pH so more electrostatic interactions were developed between these protonated functional groups and dye anions. While negative charge on the surface of

adsorbent was increased by enhancing pH above pH_{pzc} . So the adsorption efficiency was reduced by an increase in the pH on the alkaline side. Hereby the effect of pH on the adsorption of AR88 dye using IGSI at certain dose, 50 mg/L initial dye concentration and constant adsorption time was investigated. IGSI showed the maximum adsorption efficiency for AR88 dye in pH 4.5. The adsorption efficiency was reduced from 98.2% to 60% with increasing pH from 4.5 to 10.5. The surface showed maximum electrostatic attraction for dye anions after attained the more positive charge at optimum pH (41). The relation between adsorption time and DR% showed that as the reaction time increases, the removal efficiency is being enhanced. It is due to the fact that when dye molecules have more time in dealing with the adsorbent surface, they have more chance to be adsorbed by them. As the analysis indicated in mentioned situation of experiment, at first 60 minutes, dye removal from aqueous system is rapid. This is obvious from the slope of curves in Figures 3 and 4. After 60 minutes the slope tends to zero. It can be due to the fact that in the prime of adsorption process, the adsorbent has many sites to adsorb the dye molecules, but as the dye employs the parts on adsorbent surface, it becomes limited and a competition starts between molecules to be adsorbed by the adsorbent. The equilibrium data were best represented by the Langmuir isotherm model. According to the assumption of the Langmuir isotherm model, the adsorption of AR88 onto adsorbent occurred as a monolayer on the surface (42).

Conclusion

According to this study, it is proved that *S. indicum* seed's hull as an agro-based waste adsorbent, can be effectively employed for the removal of dye stuff AR88 from wastewaters. This adsorbent is available freely, locally and it is economic oriented. Especially in Iran and some other countries, it is very economical to be used in order to wastewater treatment due to its high amount of agricultural production. Dye removal efficiency increased as the amount of adsorbent and reaction time enhanced. Furthermore decreasing in initial dye concentration and pH caused increasing in adsorption efficiency. The isotherm data analysis proved monolayer sorption for acid dye. The SEM images for the IGSI before adsorption, showed pores and cavities which became smoother after being dye-loaded. Finally the ability of IGSI as a cheap and high efficiency adsorption source was proved and the contaminated water was refined up to 98% by the mentioned adsorbent.

Authors' contributions

Authors were participated in all aspects of this research work, like analysis, data collection, interpretation and manuscript approval.

Competing interests

The authors declare that they have no competing interests.

Ethical issues

There were no ethical issues in the preparation of present article.

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